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Alkylation process using a catalyst comprising a solid acid and a hydrogenation metal

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**ALKYLATION PROCESS USING A CATALYST COMPRISING A SOLID ACID
AND A HYDROGENATION METAL**

The present invention relates to a process for alkylating a hydrocarbon feed
5 which comprises contacting the hydrocarbon feed to be alkylated with an
alkylation agent in the presence of a catalyst comprising a solid acid and a
hydrogenation metal.

Within the framework of the present invention, the term alkylation refers to the
10 reaction of an alkylatable compound, such as an aromatic or saturated
hydrocarbon, with an alkylation agent, such as an olefin. Without limiting the
scope of the invention, we will further illustrate the invention by discussing the
alkylation of saturated hydrocarbons, in general branched saturated
hydrocarbons, with an olefin to give highly branched saturated hydrocarbons
15 with a higher molecular weight. Hydrocarbons contain no atoms other than
hydrogen and carbon.

This reaction is of interest because it makes it possible to obtain, through the
alkylation of isobutane with an olefin containing 2-6 carbon atoms, an alkylate
which has a high octane number and which boils in the gasoline range. Unlike
20 gasoline obtained by cracking heavier petroleum fractions such as vacuum gas
oil and atmospheric residue, gasoline obtained by alkylation is essentially free
of contaminants such as sulfur and nitrogen and so has clean burning
characteristics. Its high anti-knock properties, represented by the high octane
number, lessen the need to add environmentally harmful anti-knock compounds
25 such as aromatics or lead. Also, unlike gasoline obtained by reforming naphtha
or by cracking heavier petroleum fractions, alkylate contains few if any
aromatics or olefins, which, environmentally speaking, is a further advantage.

The alkylation reaction is acid-catalyzed. At present, in commercial alkylation
30 equipment use is made of liquid acid catalysts such as sulfuric acid and
hydrogen fluoride. The use of such catalysts is attended with a wide range of
problems. For instance, sulfuric acid and hydrogen fluoride are highly corrosive,

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so that the equipment used has to meet high quality requirements. Since the presence of highly corrosive materials in the resulting fuel is objectionable, the remaining acid has to be removed from the alkylate. Also, because of the phase separations which have to be carried out, the process is complicated and thus
5 expensive. Besides, there is always the risk that toxic substances such as hydrogen fluoride will be emitted.

A newer development in this field is the use of solid acid catalysts, such as zeolite-containing catalysts. WO 98/23560 discloses the use of a catalyst
10 containing a zeolite, such as a Y-zeolite, a Group VIII noble metal, e.g. platinum or palladium, as hydrogenation metal, and optionally a matrix material, such as alumina, in the alkylation of hydrocarbons.

In contrast to the alkylation of aromatic hydrocarbons, in the alkylation of
15 saturated hydrocarbons hydrogen transfer is the rate determining step. Hence, catalysts for the alkylation of saturated hydrocarbons require a hydrogenation metal.

It has now been surprisingly found that the use of a catalyst comprising a solid
20 acid and a hydrogenation metal and which additionally contains 1.5 - 6 wt% of water – measured as the loss on ignition (LOI) at 600°C and based on the total weight of the catalyst composition – results in a higher activity and a higher alkylate quality compared with a comparable but drier catalyst.

25 *The catalyst*

The catalyst, when used in the alkylation process, comprises 1.5 - 6 wt%. Preferably, the water content of the catalyst is 1.8 - 4 wt%, more preferably 2 - 3 wt%.

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The water content of the catalyst is its water content during use in the alkylation process and is measured by determining the weight loss upon heating the catalyst for two hours at 600°C (LOI₆₀₀).

- 5 The catalyst to be used in the process according to the invention further comprises a hydrogenation metal. Examples of suitable hydrogenation metals are constituents of the transition metals, such as metals of Group VIII of the Periodic Table, and mixtures thereof. Among these, noble metals of Group VIII of the Periodic Table are preferred. Platinum, palladium, and mixtures thereof
10 are especially preferred. The amount of hydrogenation metal will depend on its nature. When the hydrogenation metal is a noble metal of Group VIII of the Periodic Table, the catalyst generally will contain in the range of 0.01 to 2 wt.% of the metal, preferably 0.1-1 wt.%, calculated as metal and based on the total weight of the catalyst.

15

- The catalyst further comprises a solid acid. Examples of solid acids are zeolites such as zeolite beta, MCM-22, MCM-36, mordenite, X-zeolites and Y-zeolites, including H-Y-zeolites and USY-zeolites, non-zeolitic solid acids such as silica-alumina, sulfated oxides such as sulfated oxides of zirconium, titanium, or tin,
20 mixed oxides of zirconium, molybdenum, tungsten, phosphorus, etc., and chlorinated aluminium oxides or clays. Preferred solid acids are zeolites, including mordenite, zeolite beta, X-zeolites and Y-zeolites, including H-Y-zeolites and USY-zeolites. Mixtures of solid acids can also be employed. An even more preferred solid acid is Y-zeolite with a unit cell size of 24.34 - 24.72
25 angstroms, while Y-zeolite with a unit cell size of 24.42-24.56 angstroms is preferred most.

- The catalyst may additionally comprise a matrix material. Examples of suitable matrix materials are alumina, silica, titania, zirconia, clays, and mixtures thereof.
30 Matrix materials comprising alumina are generally preferred.

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Preferably, the catalyst comprises 2-98 wt% of the solid acid and 98-2 wt% of the matrix material, based on the total weight of the solid acid and the matrix material present in the catalyst. More preferably, the catalyst comprises 10-90 wt% of the solid acid and 90-10 wt% of the matrix material, based on the total weight of the solid acid and the matrix material contained in the catalyst. Even more preferably, the catalyst comprises 10-80 wt% of matrix material and balance solid acid, most preferably it comprises 10-40 wt% of the matrix material and balance solid acid, based on the total weight of the solid acid and the matrix material contained in the catalyst.

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The catalyst preferably contains no halogen component.

Preferably, the catalyst comprises catalyst particles wherein the ratio between (i) the volume in catalyst pores with a diameter of 40 – 8,000 nm (in the following "macropores") and (ii) the specific length of the catalyst particles is in the range of 0.01 - 0.90 ml/(g*mm) and wherein the catalyst has a total pore volume of at least 0.20 ml/g.

The specific length of a catalyst particle is defined as the ratio between the geometric volume and the geometric surface of the solid part of this catalyst particle. The determination of the geometric volume and the geometric surface is known to the person skilled in the art and can be carried out, e.g., as described in DE 2354558.

The macropore volume as well as the total pore volume is determined via mercury intrusion on the basis of the Washburn equation covering pores with a diameter of 3.6-8,000 nm.

Preferably, the ratio between the volume in macropores and the specific length is above 0.20 ml/(g*mm), more preferably above 0.30 ml/(g*mm), and even more preferably above 0.40 ml/(g*mm), as well as preferably below 0.80 ml/(g*mm).

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It is further preferred that the catalyst has a total pore volume of at least 0.23 ml/g and most preferably of at least 0.25 ml/g.

The catalyst particles comprised in the catalyst preferably have a specific length of at least 0.10 mm, more preferably of at least 0.16 mm, and most preferably of at least 0.20 mm. The upper limit of the specific length preferably lies at 2.0 mm, more preferably at 1.0 mm, and most preferably at 0.6 mm.

The volume in macropores preferably is at least 0.05 ml/g, most preferably at least 0.08 ml/g, and preferably below 0.30 ml/g, most preferably below 0.25 ml/g.

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The particles of the catalyst can have many different shapes, including spheres, cylinders, rings, and symmetric or asymmetric polylobes, for instance tri- and quadrulobes. Preferably, the catalyst particles have an average particle diameter of at least 0.5 mm, more preferably of at least 0.8 mm, and most preferably of at least 1.0 mm. The upper limit of the average particle diameter preferably lies at 10.0 mm, more preferably at 5.0 mm, even more preferably at 3.0 mm.

Preparation of the catalyst

20 The catalyst used in the process according to the invention is prepared by adjusting the water content of an existing catalyst comprising a solid acid and a hydrogenation metal.

The existing catalyst can be prepared by processes common to the industry. These will comprise, say, shaping the solid acid constituent after mixing it with a matrix material, to form carrier particles, followed by calcination of the particles. 25 The hydrogenating function may, e.g., be incorporated into the catalyst composition by impregnating the carrier particles with a solution of a hydrogenation metal component.

After impregnation the catalyst is preferably calcined.

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The catalyst is reduced at a temperature preferably in the range 200 to 500°C, more preferably 250 to 350°C, in a reducing gas such as hydrogen. This reduction can be performed before adjustment of the water content, after addition of water to the catalyst and/or by using reduction as a way to adjust the water content (see below). Preferably, the reduction is performed before adjustment of the water content. More preferably, the reduction is performed after drying the catalyst in a dry, non-reducing gas (N₂, He, air, etc.).

The water content of the catalyst can be adjusted by various methods. Such methods are exemplified below as methods 1, 2, and 3.

Method 1 involves increasing the LOI of a catalyst by exposing the catalyst to water. This can be achieved by exposing the catalyst to a water-containing atmosphere - e.g. air - at, e.g., ambient conditions. Embodiments of this method include:

- exposing a reduced catalyst to water until the desired LOI is reached,
- exposing an unreduced catalyst to water until an LOI above the desired level is reached, followed by reduction of the catalyst, thereby decreasing the LOI to the desired level,
- exposing a reduced catalyst to water until an LOI above the desired level is reached, followed by treatment of the catalyst in either an inert or a reducing atmosphere, thereby decreasing the LOI to the desired level, and
- reducing the catalyst in a hydrogen and water-containing atmosphere.

Method 2 involves decreasing the LOI of an existing catalyst to the desired level by reducing an unreduced catalyst with an LOI above the desired level.

Method 3 involves *in-situ* water addition by starting the alkylation process with a catalyst having an LOI below the desired level and adding water to the alkylation unit during processing, for instance by adding water to the

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hydrocarbon feed, by regenerating the catalyst in a water-containing atmosphere and/or by exposing the regenerated catalyst to a water-containing atmosphere.

- 5 A combination of two or more of the above methods is also possible.

The alkylation process

Preferably, the hydrocarbon to be alkylated in the alkylation process is a branched saturated hydrocarbon such as an isoalkane having 4-10 carbon
10 atoms. Examples are isobutane, isopentane, isohexane or mixtures thereof, with isobutane being most preferred. The alkylation agent preferably is an olefin having 2-10 carbon atoms, more preferably 2-6 carbon atoms, still more preferably 3-5 carbon atoms, and most preferably 4 carbon atoms. Most preferably, the alkylation process consists of the alkylation of isobutane with
15 butenes.

As will be evident to the skilled person, the alkylation process can take any suitable form, including fluidized bed processes, slurry processes, and fixed bed processes. The process can be carried out in a number of beds and/or reactors,
20 each with separate addition of alkylation agent if desirable. In such a case, the process of the invention can be carried out in each separate bed or reactor.

As mentioned above, water may be added during the process in order to increase the LOI of the catalyst to the desired level. This water can be
25 introduced during the alkylation reaction via, e.g., the hydrocarbon feed or the feed of alkylation agent. Alternatively, the catalyst can be hydrated by using a water-containing atmosphere during the optional (mild) regeneration steps described below, or by contacting the catalyst with water in a separate intermediate hydration step.

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Similar procedures can be applied to rehydrate the catalyst after its LOI has decreased during processing (i.e. during the alkylation reaction and/or regeneration).

- 5 Suitable process conditions are known to the skilled person. Preferably, an alkylation process as disclosed in WO 98/23560 is applied. The process conditions applied in the present process are summarized in the following Table:

	Temperature range [°C]	Pressure range [bar]	Molar ratio of hydrocarbon to alkylation agent
Preferred	-40 – 250	1 – 100	5:1 – 5,000:1
More preferred	20 – 150	5 – 40	50:1 – 1,000:1
Most preferred	65 – 95	15 – 30	150:1 – 750:1

- 10 Optionally, in the above process the catalyst may be subjected to a high-temperature regeneration with hydrogen in the gas phase. This high-temperature regeneration is preferably carried out at a temperature of at least 150°C, more preferably at 150° - 600°C, and most preferably at 200° - 400°C. For details of this regeneration procedure, reference is made to WO 98/23560, and in particular to page 4, lines 12-19. This text passage is incorporated herein by reference. The high-temperature regeneration can be applied periodically during the alkylation process.

15 If as a result of high-temperature regeneration the water content of the catalyst has decreased to below the desired level, the catalyst may be rehydrated during the process in the ways described above.

20 Preferably, in addition to the high-temperature regeneration treatment a milder regeneration is applied during the alkylation process, such as described in WO 98/23560, in particular page 9, line 13 through page 13, line 2. This text passage is incorporated herein by reference. More in particular, during the

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alkylation process the catalyst is preferably subjected intermittently to a regeneration step by being contacted with a feed containing a hydrocarbon and hydrogen, with said regeneration preferably being carried out at 90% or less, more preferably at 60% or less, even more preferably at 20% or less, and most preferably at 10% or less of the active cycle of the catalyst. The active cycle of the catalyst is defined as the time from the start of the feeding of the alkylation agent to the moment when, in comparison with the alkylation agent added to the catalyst-containing reactor section, 20% of the alkylation agent leaves the catalyst-containing reactor section without being converted, not counting isomerization inside the molecule.

The quality of the alkylate product obtained in the process according to the invention can be measured by its Research Octane Number (RON). The RON is a measure of the anti-knock rating of gasoline and/or gasoline constituents. The higher the RON, the more favourable the anti-knock rating of the gasoline will be. Depending on the type of gasoline engine, generally speaking a higher anti-knock rating is of advantage when it comes to the working of the engine. The product obtained in the process according to the invention preferably has a RON of 90 or higher, more preferably of 92 or higher, most preferably 94 or higher. The RON is obtained by determining, e.g. via gas chromatography, the percentages by volume of the various hydrocarbons in the product. The percentages by volume are then multiplied by the RON contribution and added up.

Examples of compounds with a RON of 90 or higher are isopentane, 2,2-dimethyl butane, 2,3-dimethyl butane, trimethyl butane, 2,3-dimethyl pentane, 2,2,4-trimethyl pentane, 2,2,3-trimethyl pentane, 2,3,4-trimethyl pentane, 2,3,3-trimethyl pentane, and 2,2,5-trimethyl hexane.

A related relevant parameter for product quality is the ratio of the amount of formed trimethyl pentanes (TMP) to the amount of formed dimethyl hexanes

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(DMH). Trimethyl pentanes have a RON of about 100-110. Dimethyl hexanes have a RON of about 60-70. Consequently, to obtain an alkylate with a high octane number, the highest possible TMP/DMH ratio is desired. The process according to the invention makes it possible to obtain a product having a
5 TMP/DMH ratio of at least 2, preferably of at least 3, more preferably of at least 4.

As will be shown by the Examples below, the at least 1.5 wt% of water present on the catalyst results in an increase in RON and in activity such as allows the
10 use of lower reaction temperatures to obtain the same conversion level.

FIGURES

Figure 1 illustrates the RON at 99.5% conversion and the reaction temperature required for obtaining 99.5% conversion as a function of catalyst's LOI₆₀₀ during
15 reaction.

Figure 2 displays the RON and the conversion as a function of the reaction temperature for catalysts with an LOI₆₀₀ of about 2 wt%, prepared in different ways.

20 EXAMPLES

General test procedure

A fixed-bed recycle reactor as described in WO 9823560 having a diameter of 2 cm was filled with a 1:1 volume/volume mixture of 38.6 grams of catalyst
25 extrudates and carborundum particles (60 mesh). At the centre of the reactor tube a thermocouple of 6 mm in diameter was arranged. The reactor was
flushed with nitrogen for 30 minutes (21 NI/hour). Next, the system was tested for leakages at elevated pressure, after which the pressure was raised to 21 bar
and the nitrogen replaced by hydrogen (21 NI/hour). The reactor temperature
30 was then raised to 275°C at a rate of 1°C/min and the catalyst was reduced at

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275°C. After 2 hours, the reactor temperature was lowered to the reaction temperature.

The hydrogen stream was stopped with the attaining of the reaction temperature. Isobutane was supplied to the reactor at a rate of about 4,000 grams/hour. About 95 - 98% of the isobutane was fed back to the reactor. About 2 - 5% was drained off for analysis. Such an amount of isobutane was supplied to the reactor as to ensure a constant quantity of liquid in the system. When the system had stabilized, such an amount of cis-2-butene was added to it as to give a cis-2-butene-WHSV of 0.19 (calculated on zeolite weight in the catalyst sample). The overall rate of flow of liquid in the system was maintained at about 4,000 g/h. The weight ratio of isobutane to cis-2-butene at the reactor inlet was about 750. The pressure in the reactor amounted to 21 bar.

Each time after 1 hour of reaction, the catalyst was regenerated by being washed with isobutane for 5 minutes, followed by 50 minutes of regeneration through being contacted with a solution of 1 mole% of H₂ in isobutane, and then being washed with isobutane for another 5 minutes (total washing and regeneration time 1 hour). After this washing step, alkylation was started again. The temperature during the washing steps, the regeneration step, and the reaction step was the same.

After processing as above for 24 hours at the same temperature, a pseudo-steady state was reached. Then, the temperature was decreased and the process was conducted as above for another 24 hours. Hence, the catalytic performance was measured at various temperatures going from higher to lower.

The performance was characterized by the olefin conversion per reactor pass and the research octane number (RON). The RON was determined as described on pages 13 and 14 of WO 9823560, the only exception being that the RON contribution of total C₉+ (excl. 2,2,5-trimethylhexane) was estimated

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to be 84 instead of 90. The C5+ alkylate yield is defined as the weight amount of C5+ alkylate produced divided by the overall weight of olefin consumed.

5 The LOI of the catalyst was measured by measuring the catalyst's weight loss after heating for two hours at 600°C.

Example 1

10 A calcined catalyst comprising 70 wt% USY-zeolite, 0.34 wt% platinum, and 30 wt% alumina was contacted with ambient air for different time periods in order to increase the LOI₆₀₀ to various levels ranging from 1.7 to 10.1 wt%.

The resulting catalysts were reduced at 275°C according to the general test procedure.

15 The reduced catalysts were tested in the alkylation of isobutane according to the general test procedure, using reaction temperatures up to 70°C.

After the tests, the reactor was unloaded under an inert atmosphere and the LOI₆₀₀ of the catalyst was measured, thereby correcting the weight loss for the amount of coke on the catalyst. A Leco® analyzer was used to measure the coke content. This apparatus burns the coke and measures the amount of CO₂ 20 formed. The so-corrected LOI₆₀₀ of the catalysts ranged from 1.7 to 5.0.

Experiments established that the LOI₆₀₀ does not change significantly during the alkylation reaction at the conditions used. Hence, the LOI₆₀₀ measured after the reaction is considered to be the LOI₆₀₀ during the alkylation reaction.

25 The RON at 99.5% conversion and the reaction temperature required for obtaining 99.5% conversion are plotted against the catalyst's LOI in Figure 1.

30 This figure clearly shows that the higher the water content of the catalyst, the higher the RON (i.e. the higher the selectivity) and the lower the temperature required for obtaining 99.5% conversion (i.e. the higher the activity) will be.

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Further, this figure also shows that there is an optimum in performance at an LOI between 4 and about 6 wt%.

Example 2

- 5 A calcined catalyst comprising 70 wt% USY-zeolite, 0.34 wt% platinum, and 30 wt% alumina was reduced at 275°C in the manner described in the general test procedure. Then, the catalyst was unloaded from the reactor under an inert atmosphere, separated from the carborumdum, and exposed to air until about 2 wt% of water was picked up.
- 10 The catalyst was again introduced into the reactor, flushed with hydrogen at 80°C (at which temperature essentially no water will be lost from the catalyst), and the alkylation reaction was started by supplying isobutene to the reactor, according to the general test procedure.

Several experiments were conducted, each at a different temperature.

- 15 The RON and the conversion are plotted as a function of the reaction temperature in Figure 2.

Example 3

- 20 A calcined catalyst comprising 70 wt% USY-zeolite, 0.34 wt% platinum, and 30 wt% alumina was reduced at 275°C in the manner described in the general test procedure. Then, the catalyst was unloaded from the reactor under an inert atmosphere, separated from the carborumdum, and exposed to air until 7.7 wt% of water was picked up.

- 25 The catalyst was again introduced into the reactor, and reduced again at 275°C in the manner described in the general test procedure. This resulted in a decrease of the LOI to about 2 wt%. Next, the alkylation reaction was started by supplying isobutene to the reactor, according to the general test procedure.

Several experiments were conducted, each at a different temperature.

- 30 The RON and the conversion are plotted as a function of the reaction temperature in Figure 2.

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Example 4

A calcined catalyst comprising 70 wt% USY-zeolite, 0.34 wt% platinum, and 30 wt% alumina was contacted with ambient air to obtain an LOI_{600} of about 4.1 wt%. The catalyst was then reduced and tested according to the general test
5 procedure. The LOI_{600} after reduction and before starting the alkylation reaction amounted about 2 wt%.

Several experiments were conducted, each at a different temperature.

The RON and the conversion are plotted as a function of the reaction temperature in Figure 2.

10

From Figure 2 it can be seen that the highest conversion and the highest RON are obtained with a catalyst wetted according to Example 2, while a catalyst wetted according to Example 4 shows the lowest activity and RON.

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CLAIMS

1. A process for alkylating a hydrocarbon feed which comprises contacting the hydrocarbon feed to be alkylated with an alkylation agent in the presence of
5 a catalyst comprising a solid acid, a hydrogenation metal, and 1.5 - 6 wt% of water, measured as the loss on ignition at 600°C.
2. A process according to claim 1 wherein the catalyst comprises 1.8 - 4 wt%
10 of water.
3. A process according to claim 2 wherein the catalyst comprises 2 - 3 wt% of water.
4. A process according to any one of the preceding claims wherein the solid
15 acid is selected from the group consisting of zeolites, silica-alumina, sulfated oxides, mixed oxides of zirconium, molybdenum, tungsten, or phosphorus, chlorinated aluminium oxides or clays, and mixtures thereof.
5. A process according to claim 4 wherein the solid acid is a zeolite selected
20 from the group consisting of mordenite, zeolite beta, X-zeolites, and Y-zeolites.
6. A process according to any one of the preceding claims wherein the
25 hydrogenation metal is a Group VIII noble metal.
7. A process according to any one of the preceding claims wherein the hydrocarbons are saturated hydrocarbons.

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8. A process according to any one of the preceding claims wherein the catalyst is prepared by adding water to a dry catalyst comprising solid acid and hydrogenation metal before use in the alkylation process.
- 5 9. A process according to any one of claims 1-6 wherein the alkylation process is started using a catalyst comprising less than 1.5 wt% water and wherein water is added to the catalyst during the alkylation process.

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ABSTRACT

The invention relates to a process for alkylating a hydrocarbon feed which comprises contacting the hydrocarbon feed to be alkylated with an alkylation
5 agent in the presence of a catalyst comprising a solid acid, a hydrogenation metal, and 1.5 - 6 wt% of water, measured as the loss on ignition at 600°C.

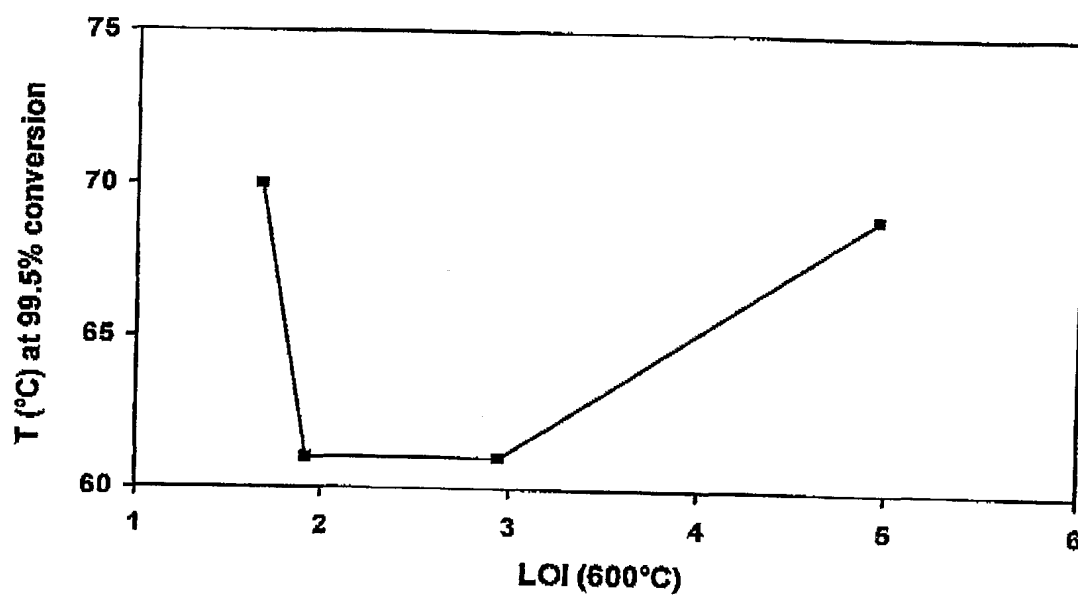
The presence of 1.5 - 6 wt% of water results in a higher activity and a higher alkylate quality compared with a comparable but drier catalyst.

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Figure 1/2



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Figure 2/2

